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# GREENHOUSE GASES PRODUCTION POTENTIAL DURING ANAEROBIC BIODIGESTION OF MANURE FROM CATTLE FED WITH DIFFERENT FEED ADDITIVES AND THEIR COMBINATIONS

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## ABSTRACT

Manure management, particularly anaerobic digestion, is an alternative for reducing the environmental impacts of cattle raising and energy generation. The aim of this study was to produce biogas and biofertilizer from waste from Nellore cows fed sodium monensin, essential oils, exogenous enzymes, and their combinations. The experimental batch-type biodigesters were placed inside a climatic chamber (30–35 °C). They were organized in a completely randomized design in a  $2 \times 2 \times 2$  factorial arrangement, with waste tested from Nellore cows fed the presence or absence of essential oil, exogenous enzyme, and monensin, with four repetitions totaling 32 experimental units (represented by the manure of the animals that received the different additives and their associations). The use of monensin reduced the amount of N inserted into the biodigesters, reduced the nutrient removal efficiency, and reduced biogas production by 39.26%, in addition to altering the composition of the biofertilizer produced. The other tested additives together with the combination of additives did not influence the biodigestion process. Therefore, the addition of monensin reduces nutrient removal efficiency, compromises biogas production, and reduces the concentration of nutrients in the biofertilizer, while essential oils and enzymes do not

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affect the biodigestion process. In addition, no associative effect was observed among the tested additives.

Keywords: Biogas, Enzyme, Essencial oil, Methane, Monensin

## **1. INTRODUCTION**

Agriculture is a significant source of greenhouse gas (GHG) emissions worldwide, accounting for 10%-12% of global anthropogenic GHG emissions. When analyzing non-carbon dioxide (CO<sub>2</sub>) emissions, enteric fermentation of ruminants is the main contributor to approximately 30%-40% of agricultural emissions, followed by the emission of waste deposited in pastures, responsible for approximately 15% of agricultural emissions (1), which can represent up to 27% of the total emissions of methane gas (CH<sub>4</sub>) by ruminants (2; 3) in intensive production systems, where these wastes accumulate in small areas.

Due to this, the correct management of animal waste becomes an important tool to reduce environmental impacts, with anaerobic biodigestion being a promising alternative, as in addition to reducing GHG emissions, it is capable of recycling waste in the form of biofertilizers, in addition to producing biogas, which is considered an alternative source of energy.

Anaerobic biodigestion can be defined as a complex interaction of microorganisms that degrade organic components present in waste, mainly in the form of CH4 and CO2 (4). In this interaction, the nutrients contained in the waste ensure the survival and reproduction of microorganisms, allowing the degradation of the organic fraction into the form of biofertilizers as well as the production of biogas (5).

Bovine waste is a suitable substrate for anaerobic biodigestion (6). However, several factors can change the characteristics of waste and influence its potential for biogas production, including animal feed (7; 8). Among all these factors, the composition of the material directly influences its degradation potential. Therefore, the extent of biogas production is dependent on animal feed. To increase the feed efficiency of ruminants and reduce the CH<sub>4</sub> emissions, several studies have reported a wide variety of nutritional techniques aimed at manipulating the ruminal environment to increase ruminant feed additives. In addition to acting in the manipulation of the ruminal environment, it can affect the use of nutrients and, consequently, the characteristics of waste excreted by animals.

Ionophores can increase the apparent energy digestibility by 2% and the apparent nitrogen digestibility by 3.5% (9). Some studies have also demonstrated that the action of essential oils makes the digestive process of food more efficient, increasing the digestibility of dry matter (DM), organic matter (OM), and neutral detergent fiber (NDF) (10). Enzyme supplementation has the main goals of removing or destroying antinutritional factors and increasing the total digestibility

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of the diet (11; 12). Furthermore, improvement in nutrient digestibility with the addition of enzyme preparations in ruminant feed has been demonstrated by several studies (13; 14; 15).

Therefore, it is expected that an increase in the digestibility of nutrients in the diet will result in changes in the composition of waste excreted by animals and, therefore, influence anaerobic digestion and, consequently, the production of biogas. Therefore, this study aimed to evaluate the potential for biogas production and the characteristics of biofertilizer from waste from Nellore cows fed with sodium monensin, essential oils, exogenous enzymes, and their combinations, as an alternative for the management of waste from cattle.

## 2. MATERIAL AND METHODS

## 2.1 Study location and ethical issues

This research project was conducted at the College of Veterinary Medicine and Animal Science of the University of São Paulo (USP), Campus Fernando Costa, and Pirassunga/SP, Brazil. The project was approved and authorized in accordance with the norms of the National Council for the Control of Animal Experimentation (CONCEA) by the Ethics Committee in the Use of Animals, Faculty of Animal Science and Food Engineering, University of São Paulo – FZEA/USP (CEUA/FZEA), filed under CEUA No. 4788111017.

## 2.1.1 Treatments and experimental design

The experiment was carried out in two phases: the feeding phase and the anaerobic digestion phase, as follows:

## 2.1.1.1 Feeding phase

Eight non-pregnant and non-lactating Nellore bovine females, with an average live weight of 480  $\pm$  55 kg, were housed individually and covered with sand beds, cement troughs, and automatic drinking fountains.

The animals were divided into two contemporary  $4 \times 4$  Latin squares in a  $2 \times 2 \times 2$  factorial arrangement and fed daily (8:00 and 16:00 h) using isoenergetic and isoprotein diets, which differed according to the presence or absence of the tested additives. Being: diet without the addition of essential oil (OE-A); diet added with 31.7 mg/kg DM of an essential oil blend composed of 43% cinnamaldehyde and 7% garlic oil (OE-P); diet without added enzyme (EN-A); diet with the addition of 1027 mg/kg DM product containing an "enzyme blend" composed of cellulase, xylanase, amylase, protease, phytase, beta-glucanase and pectinase (EN-P); diet without added monensin (MA); diet with the addition of 30.6 mg of sodium monensin/ kg DM (MP). This phase was divided into four periods of 22 days, with 16 days for adaptation to experimental diets and 5 days for fecal collection. Urine collection was carried out on the 22nd day of each period.

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Feces were collected manually through the rectum at 8:00 am and 4:00 pm, frozen at -20°C, and pooled to form a single composite sample for each animal in each period. Urine samples were obtained every 6 h during stimulation by vulvar massage and then stored at -20°C in a single vial, which formed a single composite sample within 24 h. Next, enhance (43% cinnamaldehyde + 7% garlic oil) (Novus International Inc., Indaiatuba, Brazil) was used as the source of essential oil, Allzyme® SSF (Alltech Inc., Nicholasville, USA) was used as the source of the enzymatic blend, and Rumenpac® (Grupo MCassab, São Paulo, Brazil) was used as the source of sodium monensin.

## 2.1.1.2 Anaerobic digestion phase

## 2.1.1.2.1 Substrate preparation, experimental design, and treatments

Fecal and urine samples, collected and frozen in the feeding phase, were thawed and diluted in water. A mixture of feces and urine (waste) was prepared using a theoretical ratio of 83%:17%, respectively. Then, this mixture was diluted with water and, finally, the inoculum was added.

Batch-type benchtop biodigesters were used, and 3 kg of substrate were prepared, of which 2 kg were used to fill the biodigesters and 1 kg to carry out the substrate characterization analyses (Table 1).

The substrate composition was done with the following proportions: 40% manure, 3.3% inoculum and 56.7% water. The sludge from the bovine manure treatment pond was used as an inoculum, which presented 0.164% of total solids (TS). Thus, the substrates were prepared in order to guarantee an estimate of 6% of TS.

The biodigesters were arranged in a completely randomized design in a  $2 \times 2 \times 2$  factorial scheme with 4 replications, totaling 32 experimental units (represented by the manure of the animals that received the different additives and their associations).

## 2.1.1.2.2 Biogas Production

Anaerobic biodigestion was performed under mesophilic conditions (30 to 35°C), ideal for digestion kinetics (16). The biodigesters were placed inside a climatic chamber with an electrical resistance heating system and a digital temperature controller.

The batch-type biodigesters consisted of three straight cylinders with diameters of 15, 10, and 7.5 cm, with an average capacity to ferment 2 liters of substrate each, according to (17).

The reading of biogas production was performed according to the accumulation in the gasometer. It consisted of measuring the height with a ruler fixed to the gasometer, according to its vertical displacement. The reading value was multiplied by the internal cross-sectional area of the gasometer. After each reading, the gasometers were emptied using the biogas discharge log. The

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correction of the biogas volume for conditions of 1 atm at 20°C was performed according to the methodology described by (18). To correct the volume of biogas, the expression resulting from the combination of the Boyle and Gay-Lussac laws was used:

(V0P0) / T0 = (V1P1) / T1

Where:  $V0 = corrected biogas volume, m^3 ou L; P0 = corrected biogas pressure, 10322.27 mm H_2O; T0 = corrected biogas temperature, 293.15 K; V1 = gas volume in the gas meter; P1 = biogás pressure at the time of reading, 10344.11 mm H_2O; T1 = biogas temperature, in K, at the time of reading.$ 

Considering the mean atmospheric pressure of Pirassununga equal to  $10273.11 \text{ mm H}_2\text{O}$  and the pressure given by the gasometers of 71 mm H<sub>2</sub>O, the following expression was obtained to correct the volume of biogas:

$$V0 = (V1/T1) \times 293.7703$$

Biogas samples were taken together with the measurement of the biogas volume. Samples were collected using a 60 mL syringe connected to the gas register at the top of the gasometer. Before the sampling itself, the biogas was collected and used to flush the bottle (twice), after which 50 mL of biogas were injected to analyze its composition. After collecting the biogas, the gasometers were emptied; this allowed a new accumulation of gases. The test was terminated when biogas production ceased, which occurred 164 days after filling the biodigesters.

The concentration of CH<sub>4</sub>, CO<sub>2</sub>, and N<sub>2</sub>O was determined by gas chromatography (Trace 1300, Thermo Fisher Scientific®, Rodano, Milan, Italy) in a temperature-controlled environment (25°C), according to (19). The biogas samples were diluted in glass flasks, with known volume, 16.78 times in atmospheric air. Then, 6 mL was injected into the chromatograph injector (split/splitless), of which 4 mL was used for flushing the injection system, and 2 mL was used for analysis. The system with flame ionization detector (FID) is responsible for measuring CO<sub>2</sub> and CH<sub>4</sub> and the system with electron capture detector (ECD) is responsible for the quantification of N<sub>2</sub>O.

The chromatograph was calibrated with 3.1% CH<sub>4</sub>, 3.1% CO<sub>2</sub> and 0.49% N<sub>2</sub>O diluted in atmospheric air. Two gas mixtures were used as reference, one with 50% CH<sub>4</sub> and 50% CO<sub>2</sub> and the other with 10% N<sub>2</sub>O in equilibrium with He (mol/mol).

The volumes of CH<sub>4</sub>, CO<sub>2</sub> and N<sub>2</sub>O produced ( $m^3$  or L) were calculated using the biogas production and composition data from each digester according to the equation:

$$Vol = (VolBIOGAS \times \%Gas)/100$$

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Where: Vol = volume ( $m^3$  ou L); VolBIOGAS = volume of biogas produced ( $m^3$  ou L);% Gas = contente gas of interest in biogas (%)

The production of  $CH_4$ ,  $CO_2$  or  $N_2O$  was calculated by dividing the total production of each gas by the amount of VS added or removed (difference between SV added in the filling time of the biodigesters and VS eliminated during fermentation).

The Gompertz model was used to study the kinetics of biogas and its components production. (20), according to the equation:

$$Y_t = A \exp \left[-B \exp \left(-kt\right)\right]$$

Where:  $Y_t$ : gas production (L/g VS added) at time t (day); A: model asymptote, indicates the production stabilization value (L/g VS added) in relation to time t;B: integration constant, no biological meaning.kt: maximum growth rate, logarithmic function of production growth (L/gVS added) per unit of t.

The time (t) at the inflection point was determined as follows:

$$t1 = \ln B/k$$

Where: t1: time (days) at the inflection point; ln: natural logarithm; k: production constant.

Gas production at the inflection point was determined as:

$$y1 = A/exp$$

Where: y1: gas production at the inflection point; exp: base of the natural logarithm (2.7183)

## 2.1.1.3 Removal of nutrients

The substrates added and recovered in each biodigester were weighed and multiplied by the DM percentage to calculate the DM content in grams. The added and recovered nutrients, expressed in grams, were calculated by multiplying those added or recovered and expressed in DM grams, which were expressed as a percentage and divided by 100 according to the following equation:

Nutrient (g) = Nutrient added or recovered (%) x DM (g)/100

Nutrient removal, in percentage, was calculated from the content of added and recovered nutrients and expressed in g/kg of DM according to the following equation:

Nutrient removed (%) = [Nutrient added (g) – Nutrient removed (g)] x 100/Added nutrient (g)

## 2.1.1.4 Laboratory Analysis

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The substrate samples before and after anaerobic digestion were collected, dried in an oven with ventilation and constant air renewal at 65°C for 72 hours, according to (20). Then, they were ground (1 mm) and stored in properly sealed bottles. DM was determined at 105°C for 4 hours in an oven (method 930.15; 21). Mineral matter (MM) was obtained by calcination in a muffle at 550°C for 5 hours (22). The contents of ST (ST = 100 - moisture) and SV (SV = ST - MM) of the substrates were determined with adaptations to the methodology described in (23). The total N content was determined by the micro-Kjeldahl technique (method 920.87; 22). Neutral detergent fiber (NDF) was determined by the method described by (24). The hydrogen ion potential (pH) was measured by a portable pH meter (Hanna Instruments®, HI 8424, Italy).

## 2.2 Statistical Analysis

Data were analyzed using the Statistical Analysis System (25). Before data analysis, they were evaluated for the presence of discrepant information (outliers) and normality of the residuals using the Shapiro-Wilk test. When the normality premise was not met, the data were transformed. Data were subjected to analysis of variance, which separated as causes of variation the effect of factors and their interactions, period effect, animal effect inside squared, along with squared effect. The effect of factors was analyzed using analysis of variance using 0.05 significance.

## 3. RESULTS

## **3.1 Biodigestion and nutrients removal**

The waste added to the biodigesters from animals fed with sodium monensin presented a 20.03% lower amount of N (P<0.05) than the waste from animals that did not receive such additive, with no significant difference being observed (P>0.05) for other added nutrients.

The amounts of TS and NDF remaining after the biodigestion process were 25.02% and 66.24% higher for manure from animals that received sodium monensin (P<0.05), when compared to manure from animals that did not receive sodium monensin.

The removal efficiency of TS, NDF and N were lower (P < 0.05) for biodigesters supplied with animal manure fed with sodium monensin, when compared to those supplied with animal manure that did not consume such additive (Table 1).

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	Factors								P value									
Variable	Essent	Essential Oil		Enzyme		Monensin		SEM	EO	Б	м	EO*E	EO*M	E*M	EO*E*M			
	Negative	Positive	Negative	Positive	Negative	Positive			EO	E	IVI	EO.F	EO·W	E. M	EO*E*M			
Added nutrients																		
TS, g	117.3	117.1	117.3	117.2	117.3	117.2	117.2	0.084	NS	NS	NS	NS	NS	NS	NS			
VS, g	101.1	101.6	101.4	101.4	102.0	101.8	101.4	0.448	NS	NS	NS	NS	NS	NS	NS			
FDN, g	50.82	52.14	50.47	52.48	51.16	51.79	51.53	0.913	NS	NS	NS	NS	NS	NS	NS			
N, g	5.72	5.70	5.77	5.65	6.34	5.07	5.74	0.150	NS	NS	< 0.001	NS	NS	NS	0.08			
Recovered nutrients																		
TS, g	68.68	72.86	67.81	73.73	62.9	78.64	70.38	2.158	NS	0.08	< 0.001	NS	NS	NS	NS			
VS, g	55.41	61.47	55.37	61.51	55.37	61.51	58.41	2.312	NS	NS	NS	NS	NS	NS	NS			
NDF, g	30.15	33.43	30.27	33.32	23.88	39.7	31.49	1.747	NS	NS	< 0.001	NS	NS	NS	NS			
N, g	1.92	1.99	1.87	2.04	1.99	1.92	1.95	0.055	NS	NS	NS	NS	NS	NS	NS			
Removal	efficiency																	
TS, %	41.80	38.25	42.53	37.51	46.69	33.63	40.36	1.83	NS	0.08	< 0.001	NS	NS	NS	NS			
VS, %	45.11	39.48	45.37	39.21	45.72	38.87	42.36	2.293	NS	NS	NS	NS	NS	NS	NS			
NDF, %	40.19	35	39.39	35.8	53.01	22.18	38.24	3.655	NS	NS	< 0.001	NS	NS	NS	NS			
N, %	65.50	54.09	67.01	62.58	68.3	61.3	65.12	1.545	NS	NS	0.02	NS	NS	NS	0.08			

 Table 1: Biodigestion and removal efficiency of nutrients from anaerobic batch type biodigesters supplied with waste of Nellore cows fed with essential oil, an enzyme blend, monensin and their interactions.

SEM: standard error of mean; EO: Essential Oil; E: Enzyme Blend; M: Monensin; EO\*E: Interaction between essential oil and enzyme; EO\*M: Interaction between essential oil and monensin; E\*M: Interaction between enzyme and monensin; EO\*E\*M: Interaction between essential oil, enzyme and monensin; TS: total solids; VS: volatile solids; N: nitrogen; NDF: neutral detergent fiber.

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## **3.2 Biogas Production**

Biodigesters supplied with animal waste fed with sodium monensin showed a reduction of 39.26% in biogas production (L). Consequently, lower production of CH<sub>4</sub> and CO<sub>2</sub> in absolute values (liters), 36.17% and 45.08% respectively, and relative values (L/g of feces and L/g of VS) (P<0.05) when compared to biodigesters supplied with manure from animals that did not consume this additive. However, there was no change in the composition of the biogas produced (P>0.05), which was composed of 71.92% CH<sub>4</sub>, 27.55% CO<sub>2</sub>, and 0.06% N<sub>2</sub>O, using the mean values between the factors analyzed (Table 2).

Manure from animals that consumed sodium monensin had lower (P<0.05) production rate (A) and lower (P<0.05) production at the inflection point (y) for both CH<sub>4</sub> (Figure 1) and CO<sub>2</sub> variable.

The use of sodium monensin in the diet increased the production rate (A) and production at the inflection point (y) for the N<sub>2</sub>O variable (P<0.05), however, the total production of this gas was not changed (P>0.05) (Table 2).

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			Fac	tors	P value										
Variable	Essent	ial Oil	Enz	Enzyme		Monensin		SEM				OF*	OF*	E*	OE*E*
variable	Negativ	Positiv	Negativ	Positiv	Negativ	Positiv	e	5LIVI	OE	Е	М	E	M	M	M
	e	e	e	e	e	e						-			
Biogas, L	40.46	40.29	39.86	40.89	50.24	30.51	40.58	2.40	NS	NS	<0.00 1	NS	NS	NS	NS
CH <sub>4</sub>															
CH4, L	29.22	28.79	29.11	28.91	35.41	22.6	29	1.65	NS	NS	<0.00 1	NS	NS	NS	NS
СН4, %	71.45	72.28	72.73	71.01	70.32	73.41	71.92	0.82	NS	NS	0.07	NS	NS	NS	NS
CH4/feces, L/g	0.029	0.029	0.029	0.029	0.036	0.023	0.029	0.001 6	NS	NS	<0.00 1	NS	NS	NS	NS
CH4/added VS	0.28	0.28	0.28	0.28	0.34	0.22	0.28	0.016	NS	NS	<0.00 1	NS	NS	NS	NS
A, L/g	0.32	0.3	0.3	0.31	0.35	0.26	0.31	0.014	NS	NS	0.001	NS	NS	NS	NS
k, L/g.day	0.04	0.036	0.037	0.034	0.041	0.03	0.036	0.002 9	NS	NS	NS	NS	NS	NS	NS
t, day	52.32	47.6	43.56	56.35	44.22	55.69	48.86	3.62	NS	0.09	NS	NS	NS	NS	NS
y, L/g	0.12	0.111	0.113	0.115	0.131	0.097	0.115	0.005 2	NS	NS	0.001	NS	NS	NS	NS
CH <sub>4</sub> /remove d VS, L/g CO <sub>2</sub>	0.7	0.82	0.7	0.83	0.9	0.62	0.76	0.068	NS	NS	0.05	NS	NS	NS	NS
CO <sub>2</sub> , L	11.22	11.01	10.73	11.5	14.35	7.88	11.05	0.83	NS	NS	<0.00 1	NS	NS	NS	NS
CO <sub>2</sub> , %	27.6	27.65	26.31	28.94	28.76	26.49	27.55	0.75	NS	0.09	NS	NS	NS	NS	NS
CO <sub>2</sub> /feces, L/g	0.011	0.011	0.01	0.011	0.014	0.08	0.011	0.000 8	NS	NS	<0.00 1	NS	NS	NS	NS

# Table 2: Gas production (total biogas, CH4, CO2 and N2O) in batch type biodigesters with waste of Nellore cows fed with essential oil, an enzyme blend, monensin and their interactions

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CO <sub>2</sub> /added VS	0.11	0.108	0.105	0.113	0.14	0.078	0.108	0.008 2	NS	NS	<0.00 1	NS	NS	NS	NS
A, L/g	0.12	0.116	0.112	0.123	0.143	0.092	0.121	0.008 7	NS	NS	0.006	NS	NS	NS	NS
k, L/g.day	0.036	0.034	0.037	0.033	0.042	0.028	0.037	0.003 4	NS	NS	0.09	NS	NS	NS	NS
t, day	51	47.58	42.24	56.33	44.14	54.43	47.41	3.92	NS	NS	NS	NS	NS	NS	NS
y, L/g	0.044	0.0426	0.041	0.0455	0.052	0.034	0.044	0.003 2	NS	NS	0.006	NS	NS	NS	NS
CO <sub>2</sub> /remove d VS, L/g N <sub>2</sub> O	0.27	0.318	0.257	0.331	0.368	0.221	0.294	0.029	NS	NS	0.01	NS	NS	NS	NS
$N_2O$ , mL	18.58	20.99	26.33	13.25	10.08	29.49	19.94	6.21	NS	NS	NS	NS	NS	NS	NS
N <sub>2</sub> O, %	0.056	0.061	0.071	0.047	0.017	0.1	0.059	0.02	NS	NS	0.058	NS	NS	NS	NS
N <sub>2</sub> O/feces, mL/g	0.018	0.021	0.026	0.013	0.01	0.03	0.02	0.006 3	NS	NS	NS	NS	NS	NS	NS
N <sub>2</sub> O/added VS	0.184	0.205	0.259	0.13	0.097	0.291	0.196	0.061	NS	NS	NS	NS	NS	NS	NS
A, mL/g	0.318	0.135	0.383	0.071	0.099	0.354	0.189	0.061	0.0 7	0.00 5	0.01	NS	NS	NS	NS
k, mL/g.day	0.034	0.035	0.036	0.032	0.04	0.029	0.035	0.002 7	NS	NS	0.07	NS	NS	NS	NS
t, day	55.17	47.55	46.22	56.5	44.24	58.48	49.61	3.69	NS	NS	0.06	NS	NS	NS	NS
y, mL/g	0.117	0.049	0.141	0.026	0.036	0.13	0.069	0.022	0.0 7	0.00 5	0.01	NS	NS	NS	NS
N <sub>2</sub> O/remove d VS, mL/g	0.433	0.464	0.57	0.327	0.194	0.702	0.451	0.142	NS	NS	0.1	NS	NS	NS	NS

SEM: stanadard error of mean; EO: Essential Oil; E: Enzyme Blend; M: Monensin; EO\*E: Interaction between essential oil and enzyme; EO\*M: Interaction between essential oil and monensin; E\*M: Interaction between enzyme and monensin; EO\*E\*M: Interaction between essential oil, enzyme and monensin; VS: volatile solids; A: asymptotic production (L/g added VS); k: production constant (L/g added VS per day); t: time at inflection point (day); y: production at inflection point (L/g added VS).

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# Figure 1: CH<sub>4</sub> production, adjusted by the Gompertz model, in batch-type biodigesters supplied with waste from Nellore cows, fed with or without sodium monensin.

### 3.3 Biofertilizer Composition

Waste from animals fed with sodium monensin resulted in biofertilizers with higher total carbon content (P<0.05) and lower levels of N, P<sub>2</sub>O<sub>5</sub>, and K<sub>2</sub>O (P<0.05), resulting in a higher C: N ratio without changing the amount of organic carbon (Table 22). Additionally, the biofertilizer obtained from animal waste that received sodium monensin had a lower pH value (P<0.05) (Table 3).

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				P-value											
	Essential Oil		vil Enzyme		Monensin		Averag	SEM	Б			EO*	EO*	E*	EO*E*
Variable	Negativ	Positiv	Negativ	Positiv	Negativ	Positiv	e	SLIVI		Е	Μ	EO	M	M	M
	e	e	e	e	e	e			U			Ľ	111	111	171
									Ν		< 0.00				
Total C (g/kgMS)	429.3	437.2	429.6	436.9	413.6	452.9	432.4	4.35	S	NS	1	NS	NS	NS	NS
Organic C									Ν						
(g/kgMS)	163.6	162.6	162.5	163.7	163.8	162.4	163.1	0.84	S	NS	NS	NS	NS	NS	NS
									Ν		$<\!0.00$				
Total N (g/kgMS)	27.82	27.75	28.02	27.55	31.74	23.83	27.78	0.95	S	NS	1	NS	NS	NS	NS
									Ν	0.0	$<\!0.00$				
$P_2O_5$ (g/kgMS)	18.21	18.18	18.78	17.6	20.75	15.64	18.31	0.55	S	7	1	NS	NS	NS	NS
									Ν		$<\!0.00$				
K <sub>2</sub> O (g/kgMS)	27.00	25.50	26.73	25.77	30.27	22.22	26.40	0.94	S	NS	1	NS	NS	NS	NS
									Ν		$<\!0.00$				
C/N	15.62	16.32	15.92	16.02	13.22	18.71	15.9	0.60	S	NS	1	NS	NS	NS	NS
								0.03	Ν						
pH	7.70	7.73	7.72	7.71	7.79	7.64	7.72	0	S	NS	0.02	NS	NS	NS	NS

# Table 3: Composition of biofertilizers obtained in batch type biodigesters supplied with waste from Nellore cows fed with essential oils, a blend of exogenous enzymes, sodium monensin and their associations.

SEM: stanadard error of mean; EO: Essential Oil; E: Enzyme Blend; M: Monensin; EO\*E: Interaction between essential oil and enzyme; EO\*M: Interaction between essential oil and monensin; E\*M: Interaction between enzyme and monensin; EO\*E\*M: Interaction between essential oil, enzyme and monensin; C/N: Carbon: Nitrogen ratio.

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### 4. DISCUSSION

The use of cattle waste as a substrate for anaerobic digestion is a good alternative to carbohydrate, protein, and fat (6). However, certain factors can alter the potential for biogas production. According to (26), the composition of the material directly influences the potential for degradation of the substrate. Thus, the extent of biogas production from manure is dependent on animal feed.

It is important to emphasize that different additives used as modifiers of ruminal metabolism do not decrease CH<sub>4</sub> production through a single mechanism of action. Sodium monensin is a classic manipulator of the rumen environment, directing H<sub>2</sub> that would be used for the production of CH<sub>4</sub> for the production of propionic acid, thus causing a change in ruminal patterns with increased energy efficiency (27). Essential oils such as cinnamaldehyde and garlic oil have antimicrobial properties and the potential to modulate rumen fermentation, being mostly investigated in in-vitro experiments (28; 29; 30; 31; 32; 33). Among its main advantages, the low risk of microbial resistance stands out because these compounds present, in most cases, several active principles that give different modes of action (34). Exogenous enzymes appear as alternatives that can promote improvements in digestibility and use of the offered diet. The associated use of different exogenous enzymes showed an improvement in rumen fermentation when compared to the use of isolated enzymes. Even in conditions where the rumen has a high rate of fermentation in the diet, it is still possible to observe the elimination of degradable fibers and starch in feces (35; 36). Because the feed additives mentioned above do not have a unique and exclusive mechanism of action, nothing prevents their effects from being additive - the result of the combination is equal to the sum of the parts - or even synergistic - the combined result is greater than the sum of the parts.

The use of essential oils and exogenous enzymes did not affect the nutrients added to the biodigesters or biodigestion process. Similarly, another study evaluating the effects of exogenous enzymes (37) found no significant differences in the production of gases from the feces of dairy cows. For example, cattle fed cottonseed and vitamin E added to their diets did not show significant differences in the fecal emissions of biogas,  $CH_4$ , and  $N_2O$ , with the addition of cottonseed increasing the concentration of  $CH_4$  in the feces and reducing that of  $CO_2$  but did not affect the total production of  $CH_4$ ,  $CO_2$ , and  $N_2O$  in the biodigesters. (38).

In the present study, sodium monensin did not affect the pH of the material introduced into the biodigesters or the amounts of TS, VS, and NDF added. However, this reduced the amount of N added. This reduction is justified by the ability of sodium monensin to increase the use of N in the diet (9), thereby influencing the biodigestion process. For the biodigestion process to occur under satisfactory conditions, nutrients must be present in sufficient quantities (39), with N being the main one, since during the anaerobic decomposition process, microorganisms use NH<sub>3</sub> and organic

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forms of N for their growth (40). Additionally, (41) indicates the importance of N concentration, because if the C:N ratio is not adequate, bacteria cannot consume all the carbon present, and the process performance will be low.

Despite the lower availability of N with the use of sodium monensin, the efficiency of VS removal did not change and had an average value of 42.36%, which can be considered within the appropriate range (30–45%). The composition of the biogas produced was not altered and was within the parameters presented in (42). The mixture of gases was composed of 50-80% CH<sub>4</sub> and 20-40% CO<sub>2</sub>. In the present study, the biogas produced was composed of 71.92% CH<sub>4</sub>, 27.55% CO<sub>2</sub>, and 0.06% N<sub>2</sub>O, using the mean of all the analyzed factors. However, the use of sodium monensin reduced the removal efficiency of TS and NDF, indicating lower fermentation activity, resulting in a 39.26% drop in biogas production due to the lower production of CH<sub>4</sub> and CO<sub>2</sub>. However, (43), evaluating the supplementation of monensin and Acacia mearnsii tannins in the diet of Nellore cows, observed antagonistic interactions when the additives were associated with the aim of reducing the emission of gases in the feces of these animals. According to (44), part of the monensin consumed by animals can be recovered in feces. This effect was not observed in the urine or tissues of animals. (45), when determining the pattern of excretion and tissue distribution of monensin in cattle, reported a 95% recovery of the active metabolites of monensin in the feces of animals.

The effect of cattle diet on the environmental impact caused by manure concluded that the use of ionophores in the diet delayed the start of biogas production and altered the total production (46). These results are similar to those found in the present study. In addition to lower biogas production, a lower rate of  $CH_4$  and  $CO_2$  production was observed with sodium monensin in the diet. In addition, according to (46), such a change in the biodigestion process is due to monensin being responsible for preventing the growth of acetate-producing bacteria, reducing the availability of C and H for methanogenic archaea.

The lower efficiency of TS and NDF removal observed in the biodigesters that received manure from animals fed monensin resulted in a higher concentration of TS and NDF in the remaining material (Table1). Consequently, this resulted in a higher concentration of C total in the biofertilizer obtained at the end of the process. It dilutes the amounts of N,  $P_2O_5$ , and  $K_2O$  (Table 3) because the transformation of C into CH<sub>4</sub> is responsible for concentrating the nutrients in the biofertilizer (47). Thus, the lower production of CH<sub>4</sub> and CO<sub>2</sub> in these biodigesters (Figure 1, Table 2) justifies the higher C total concentration and lower concentrations of N,  $P_2O_5$ , and  $K_2O$  in the obtained biofertilizer, consequently changing the C: N ratio and moving away from the optimal ratio of 10:13:1 in the stabilized residue (48).

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When analyzing the effluent pH, we observed that sodium monensin provided a slight drop (Table 3) but did not remove it from the ideal range between 7 and 8.5 pointed out by (49) and (50), characterizing it in terms of its basic pH as a soil pH corrector.

## **5. CONCLUSION**

The addition of sodium monensin reduces nutrient removal efficiency, compromises biogas production, and reduces nutrient concentrations in biofertilizers. Both EO and E did not affect the anaerobic biodigestion process. In addition, no associative effect was observed between the tested additives during the anaerobic biodigestion process.

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